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# Solid-Liquid Phase Equilibria for Mixtures of Lithium, Sodium, and Potassium Carbonates

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IN STUDIES on physicochemical and electrochemical aspects of molten carbonates, knowledge of the liquid-solid phase equilibria for binary and ternary systems of the alkali metal carbonates is essential. The high reactivity and thermal instability of molten alkali carbonates, and the consequent experimental problems, undoubtedly contribute in large part to uncertainties in the published data for these systems.

A comprehensive review of the knowledge of the phase equilibria up to 1958 has been recently published (2). Results for the three binary systems and the ternary system based on the use of the visual technique have recently been published by Volkova (7). While the general features of the binary liquid-solidus equilibria are qualitatively confirmed, the results contribute little to the accurate knowledge of these systems, since the data of Volkova for the liquidus temperatures, eutectic compositions, and temperatures differ appreciably from the earlier work. For the ternary system, with the exception of a passing reference by Tamaru and Kamada (6) which mentions a mixture melting at 380° C., without specifying the composition, knowledge is limited to the results of Volkova. For the Na<sub>2</sub>CO<sub>3</sub>-K<sub>2</sub>CO<sub>3</sub> solid-liquid phase equilibria, the recent publication by Reisman (4) settles the outstanding uncertainties for this binary system. This article reports the results of studies for the Li<sub>2</sub>CO<sub>3</sub>-Na<sub>2</sub>CO<sub>3</sub>, Li<sub>2</sub>CO<sub>3</sub>-K<sub>2</sub>CO<sub>3</sub>, and Li<sub>2</sub>CO<sub>3</sub>-Na<sub>2</sub>CO<sub>3</sub>-K<sub>2</sub>CO<sub>3</sub> systems undertaken to establish accurately the liquid-solid phase equilibria in mixtures.

#### EXPERIMENTAL

The  $Li_2CO_3$ ,  $Na_2CO_3$ , and  $K_2CO_3$  (analytical reagent grade chemicals) were dried to constant weight under a  $CO_2$  atmosphere at 600° C., and stored over  $P_2O_5$  in desiccators until used.

A 50-cc. gold (or gold-20% palladium alloy) crucible was used to contain the molten carbonates for the thermal analyses experiments. Preliminary corrosion tests showed that these metals suffered no attack after contact with molten carbonates for periods up to 60 hours at temperatures up to 950° C. The experimental arrangement consisted

 $O_3$ -Na<sub>2</sub>CO<sub>3</sub>urately the LiKCO<sub>3</sub>, at the approximate liquidus temperatures to define the nature of the curve accurately in the 40 to 65% Li<sub>2</sub>CO<sub>3</sub> composition region. In the Li<sub>2</sub>CO<sub>3</sub>-Na<sub>2</sub>CO<sub>3</sub> system, for compositions in the range 30 to 70% Li<sub>2</sub>CO<sub>3</sub>, even with the most careful seeding efforts, a relatively large uncertainty remained relative to the first halt temperature in the cooling curves. The maximum uncertainty is shown in Figure 1,B, by the dotted lines below the liquidus curves.

The experimental compositions investigated for the two binary systems, and the liquidus-solidus curves and eutectic halts are illustrated in Figure 1, A and B. From large-scale graphs of the results, and those of earlier contributions, a comparison of liquidus temperatures at uniform composition increments was compiled (Table I).

Data for the experimental compositions investigated, and temperatures at which inflections and halts were noted in

of the crucible supported on an alundum pedestal enclosed in a 96% silica glass tube. Alundum baffles prevented excessive heat losses. A motor-driven rotating stirrer maintained homogeneity in the melt. The low torque motor stopped automatically with thickening of the solid-liquid mixture. A gold-sheathed 96% silica glass thermocouple tube was immersed in the melt. A recording differential potentiometer (5) and a Pt-Pt, 10% Rh thermocouple were used to trace the temperature time curves. The  $\times$  20 range on this instrument, corresponding to approximately 100° C. for full scale deflection, was used to follow the temperaturetime histories for most experiments. Temperatures could readily be read to the nearest 0.1° C. Critical points were checked with the next more sensitive range (20° for full scale deflection). At all times an atmosphere of CO2 was maintained above the sample by a controlled flow of the gas into the sample housing through a 96% silica glass tube.

Various cooling rates, from 0.5° to 2.0° C. per minute, were used. At least two cooling curves for every composition point were observed: in doubtful cases as many as six indepentently prepared mixtures were investigated. Freezing points were reproducible to within 1° C. Melts were seeded to avoid excessive supercooling—i.e.,

 $> 2^{\circ}$  to  $3^{\circ}$  C. For the Li<sub>2</sub>CO<sub>3</sub>-K<sub>2</sub>CO<sub>3</sub> system, it was essential

to seed with crystals of the intermediate compound,

# electrochemical of the crucible supported on an alund the liquid-solid in a 96% silica glass tube. Alundu excessive heat losses. A motor-dr

the cooling curves for six cuts across the field of the ternary are summarized in Table II. From these data, and the knowledge of the three binary systems, a large scale model of the composition-temperature phase equilibria was constructed and the liquidus surface isothermals as illustrated in Figure 2 were developed. The composition and melting point for the apparent ternary eutectic are (mole %): Li<sub>2</sub>CO<sub>3</sub>, 43.5; Na<sub>2</sub>CO<sub>3</sub>, 31.5; and K<sub>2</sub>CO<sub>3</sub>, 25.0; m.p. 397°  $\pm$  1°C., respectively.

## DISCUSSION

Li<sub>2</sub>CO<sub>3</sub>-K<sub>2</sub>CO<sub>3</sub>. A compound LiKCO<sub>3</sub>, congruently melting at 504.5°  $\pm$  1° C. is formed. Two eutectic mixtures at 42.7 and 62.0 mole % Li<sub>2</sub>CO<sub>3</sub>, and melting at 498° and 488° C., respectively, are present. Unless the melts were seeded with crystals of LiKCO<sub>3</sub> in the region of these eutectics, the samples would cool beyond the above temperatures to a second set of eutectic halts at 460° and 465° C., respectively. This set is shown by the dotted horizontal lines in Figure 1, A. For mixtures of compositions in the region 45 to 60 mole % Li<sub>2</sub>CO<sub>3</sub>, the separation of LiKCO<sub>3</sub> was readily induced by simple cooling, without seeding.

	$\mathbf{T}_{1}, \circ \mathbf{C}.$				
Li₂CO₃,	Le Chatelier	Volkova	Present authors		
Mole $\%$	(3)	(7)			
	$Li_2CO_3$ - $K_2$	CO3 System			
0.00	860	896	899		
10.0	776	810	829		
20.0	687	716	742		
30.0	<b>6</b> 00	611	644		
40.0	511	496	533		
42.0	503	497	508		
44.0	505	498	500		
50.0	508	499	505		
60.0	504	497	503		
62.0	498	493	498		
72.0	552	552	557		
80.0	618	625	625		
90.0	671	683	683		
100.0	710	732	726		
	$Li_2CO_3$ -Na <sub>2</sub>	${}_{2}\mathbf{CO}_{3}$ System			
0.00	(858) °	860	858		
10.0	(808)	798	806		
20.0	(749)	(732)	(746)		
30.0	(683)	660	678		
40.0	(596)	585	$598 \pm 2$		
45.0	548	545	$557 \pm 3$		
48.0	(519)	520	$530 \pm 5$		
50.0	513	500	$512 \pm 512$		
52.0	(515)	500	500		
55.0	543	498	516		
60.0	576	516	544		
70.0	620	570	597		
80.0	662	624	646		
90.0	699 795	678 799	689 796		

Inspection of data in Table I shows that the present
results entirely confirm the nature of the liquidus-solidus
phase equilibria of the earlier studies of Le Chatelier $(3)$
and Volkova (7) for this system. The consistently lower
values of Volkova (at 35 mole % Li <sub>2</sub> CO <sub>3</sub> , the liquidus-
temperature is as much as 35° C. lower than that observed
in the present work) may be attributed as a consequence of
the visual method used by Volkova to detect the tempera-
tures of first crystallization and the high degree of super-

# Table II. Thermal Analysis Data for Li<sub>2</sub>CO<sub>3</sub>-Na<sub>2</sub>CO<sub>3</sub>-K<sub>2</sub>CO<sub>3</sub> System

Composition, Mole %			Crystallization Temp., ° C.				
$Li_2CO_3$	$Na_2CO_3$	K <sub>2</sub> CO <sub>3</sub>	$T_1$	$T_2$	$T_3$		
Series I							
$\begin{array}{c} 60.9 \\ 57.1 \\ 57.5 \\ 47.7 \\ 43.3 \\ 39.8 \\ 38.2 \\ 30.0 \\ 0.00 \end{array}$	$\begin{array}{c} 0.00\\ 6.3\\ 15.5\\ 21.7\\ 29.0\\ 34.7\\ 37.0\\ 50.5\\ 100 \end{array}$	$\begin{array}{c} \textbf{39.1} \\ \textbf{36.6} \\ \textbf{33.0} \\ \textbf{30.6} \\ \textbf{27.7} \\ \textbf{25.5} \\ \textbf{24.8} \\ \textbf{19.5} \\ \textbf{0.00} \end{array}$	490 476 453 436 419 475 452 568 858	· · · · · · · · · · · · ·	399 399 397 398 398 398 391		
Series II							
$\begin{array}{c} 0.00\\ 6.7\\ 12.6\\ 19.2\\ 26.0\\ 32.6\\ 48.6\\ 54.7\\ 59.8\\ 64.4\\ 68.6\\ 73.0\\ 76.4\\ 100 \end{array}$	$\begin{array}{c} 60.0\\ 56.0\\ 52.5\\ 48.5\\ 44.4\\ 40.4\\ 30.8\\ 27.1\\ 24.1\\ 21.4\\ 18.8\\ 16.2\\ 14.1\\ 0.00\\ \end{array}$	$\begin{array}{c} 40.0\\ 37.3\\ 34.9\\ 32.3\\ 29.6\\ 27.0\\ 20.6\\ 18.2\\ 16.1\\ 14.2\\ 12.6\\ 10.8\\ 9.5\\ 0.00\\ \end{array}$	$\begin{array}{c} 710\\ 669\\ 632\\ 590\\ 542\\ 492\\ 470\\ 494\\ 518\\ 549\\ 579\\ 605\\ 624\\ 726\end{array}$	451 450 450  418  417 417 417 417 415 409 	399 399 398 397 393 393 393 392 392 392 392 392 392		
Series III							
$\begin{array}{c} 0.00\\ 14.8\\ 22.3\\ 27.9\\ 33.6\\ 38.9\\ 44.4\\ 49.1\\ 53.1\\ 100 \end{array}$	$72.3 \\ 61.6 \\ 56.2 \\ 52.1 \\ 48.0 \\ 44.2 \\ 40.2 \\ 36.8 \\ 33.9 \\ 0.00$	$\begin{array}{c} 27.7\\ 23.6\\ 21.5\\ 20.0\\ 18.4\\ 16.9\\ 15.4\\ 14.1\\ 13.0\\ 0.00\\ \end{array}$	$740\\663\\617\\580\\541\\498\\448\\480\\503\\726$	 411 421 441 445 444	390 390 391 391 392 392 392 391		
Series IV							
43.1 37.5 32.8 29.7	0.00 13.0 23.9 31.2	56.9 49.5 43.3 39.1	499 462 452 475	 435 (419) 454	 390 		
23.3 17.5	46.0 59.6	30.7 22.9	648	• • •	399 390		
0.00 100 0.00 600 Series V							
58.0 47.6 40.6 36.7 43.5 0.00	$\begin{array}{c} 42.0 \\ 34.4 \\ 29.3 \\ 26.6 \\ 31.5 \\ 0.00 \end{array}$	0.00 18.0 30.1 36.7 25.0 100	$533 \\ 434 \\ 415 \\ 424 \\ \dots \\ \dots$	500  406  898	395 397  397 		
Series VI							
$\begin{array}{c} 48.7\\ 26.8\\ 19.5\\ 14.3\\ 40.8\\ 36.4 \end{array}$	$51.3 \\ 28.2 \\ 20.5 \\ 15.0 \\ 42.8 \\ 38.1$	$\begin{array}{c} 0.00\\ 45.0\\ 60.0\\ 70.7\\ 16.4\\ 25.5\end{array}$	525 510 638 725 480 465	500 420 429 	  395 397		

cooling possible on these systems. Inspection of the work of Le Chatelier (3) shows that the melting point of pure  $K_2CO_3$  is reported as 860° C., some 40° below accepted values; therefore agreement of those data with present results, except in a qualitative way, would not be anticipated.

An interesting feature in the present system is the second set of eutectic halts that are attained in a range of compositions as shown in Figure 1, A. One possibility is that  $LiKCO_3$  has a crystalline modification which is stable at lower temperatures and it is this phase which freezes out at the second set of eutectics.



Li<sub>2</sub>CO<sub>3</sub>-Na<sub>2</sub>CO<sub>3</sub>. Inspection of the thermal analysis in which Eitel and Skaliks (1) first advanced the suggestion that a congruently melting compound LiNaCO3 occurs in this system shows clearly that the limited number of experimental compositions and the scatter in the data are insufficient to support this claim. Evidence is based entirely on supporting results of x-ray analysis and index of refraction data (1) obtained from melts cooled to room temperature. Consideration of the present thermal analysis data shows clearly that the Na<sub>2</sub>CO<sub>3</sub>-Li<sub>2</sub>CO<sub>3</sub> system is of the simple eutectic type. The dotted lines (Figure 1, B) give the maximum uncertainty and rule out the separation of the congruently melting compound, LiNaCO<sub>3</sub>, previously suggested (6, 7). Although the eutectic region was investigated repeatedly, the early work (6, 7) could not be confirmed. The rather unambiguous thermal data show that the confusion in this region is due to the conclusions based on the x-ray data obtained at room temperature relative to the status of the system above this temperature. Inspection of the limited thermal data of Eitel and Skaliks (1) shows that interpretation of the results as a simple liquid-solid eutectic type diagram is possible. The thermodynamically improbable x-ray data may be interpreted equally well due to polymorphic transitions with composition and/or solid solution effects arising in the solid system on cooling from the simple eutectic system at 501° C. to room temperature. Experimental data concerning the solid state diagram of the system are required to resolve this point. The existence of a simple eutectic is strongly supported by the unambiguous thermal data for the liquidus region.

 $Li_2CO_3$ -Na<sub>2</sub>CO<sub>3</sub>-K<sub>2</sub>CO<sub>3</sub>. According to the three binary systems which bound this ternary system, the latter is expectedly complex. The present investigation is mainly concerned with the liquidus surface and not with complete accurate characterization of the ternary system. Inspection of the liquidus surface shown in Figure 2 indicates three fields of crystallization-i.e., that of Li<sub>2</sub>CO<sub>3</sub>, LiKCO<sub>3</sub>, and solid solution Na<sub>2</sub>CO<sub>3</sub>-K<sub>2</sub>CO<sub>3</sub>. At the intersection of the three lines of demarcation, there exists the lowest melting mixture of the ternary system. Interpretation of this point, m.p.  $397^{\circ} \pm 1^{\circ}$  C., composition (mole %), Li<sub>2</sub>CO<sub>3</sub>:Na<sub>2</sub>CO<sub>3</sub>:  $K_2CO_3$  is 43.5:31.5:25.0, respectively, as a simple ternary eutectic is supported by thermal data (Table II, Series V, 5th entry).

Molar ratio of the three carbonates in this mixture approximates very nearly the simple ratio: 1.00:1.25:1.75 for  $K_2CO_3:Na_2CO_3:Li_2CO_3$ . The composition of a lowmelting ternary mixture (390° C.) in this system as reported by Volkova (7) was (mole %);  $Li_2CO_3:Na_2CO_3:K_2CO_3$ ; 27:45:28. Inspection of present results shows that for a point of this composition, the first crystallization tempera-





Figure 2. Temperature isothermals for liquid-solid equilibria in the ternary Li<sub>2</sub>CO<sub>3</sub>-Na<sub>2</sub>CO<sub>3</sub>-K<sub>2</sub>CO<sub>3</sub> system

Exact composition of the ternary eutectic, m.p. 397  $\pm$  1° C., is (mole %), Li<sub>2</sub>CO<sub>3</sub>:Na<sub>2</sub>CO<sub>3</sub>:K<sub>2</sub>CO<sub>3</sub>; 43.5:31.5:25.0, respectively

ture is 480° C. (Table II, Series VI), with cooling to the ternary eutectic composition and temperature following. The erroneous composition cited by Volkova is thus understood, if the cooling curve had been initiated at temperatures less than 480° C. under which circumstances the first arrest in the cooling curve to solid phase separation would not have been observed. The somewhat lower melting points, 390° and 380° C., reported in the earlier investigations (6, 7) could not be reproduced in the present work. Errors due to supercooling effects and thermometry in the earlier studies could well account for temperature differences of this magnitude. There are insufficient details given in the original publications to resolve these points further.

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